

Solution of PDE's using Laplace

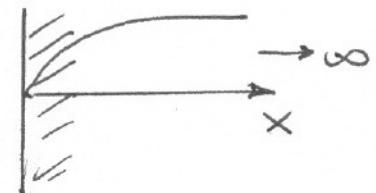
When?

- Problem cannot be solved with separation of variables
- Transform with respect to variable that goes from $0 \rightarrow \infty$
e.g. time ($0 < t < \infty$)

Motivation Example

Solve the temperature $T(x,t)$ in a semi-infinite well (very thick well)

Heat transfer in 1 dimension only:



$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial x^2} \quad (1)$$

with Boundary Conditions:

$$T(0,t) = T_0 \quad (2)$$

$$T(\infty, t) = T_b \quad (3)$$

and Initial Condition $T(x,0) = T_b \quad (4)$

Try separation of variables: $T(x,t) = f(x)g(t) \quad (5)$

$$(5) \text{ into (1)} : \quad g'f = \alpha f''g \Rightarrow \frac{g'}{g} = \frac{f''}{f} = -\lambda^2 \quad (6)$$

$$(6) \Rightarrow g = Ae^{-\lambda^2 \alpha t} \quad \text{and} \quad f = B \cos \lambda x + C \sin \lambda x$$

$$\Rightarrow \text{from (5)} \quad T(x,t) = Ae^{-\lambda^2 \alpha t} (B \cos \lambda x + C \sin \lambda x) \quad (7)$$

Can we satisfy all BC's and IC's with (7) ?

The answer is no!

$$T(\infty, t) = Ae^{-\lambda^2 \alpha t} (B \cos \alpha \infty + C \sin \alpha \infty) \text{ not defined}$$

Thus, separation of variables does not work!

Let try Laplace Transforms.

Laplace Transform Review

Definition

$$F(s) = \int_0^\infty e^{-st} f(t) dt$$

Some properties

$$\mathcal{L} \left[\frac{\partial f(x,t)}{\partial t} \right] = \int_0^\infty e^{-st} \frac{\partial f}{\partial t} dt \rightarrow \text{integration by parts}$$

$$= f(x,t) e^{-st} \Big|_{t=0}^{t=\infty} + s \int_0^\infty f(x,t) e^{-st} dt =$$

$$= s F(x,s) - f(x,0)$$

$$\mathcal{L} \left[\frac{\partial f(x,t)}{\partial x} \right] ? \text{ if Laplace is done wrt } t$$

$$= \int_0^\infty e^{-st} \frac{\partial f}{\partial x} dt = \frac{\partial}{\partial x} \int_0^\infty e^{-st} f(t) dt = \frac{\partial F(x,s)}{\partial x}$$

since s is an algebraic variable $\frac{\partial F}{\partial x} = \frac{dF}{dx}$

Continuation of Semi-infinite well example

Step 1 - Transform differential equation + B.C.'s

$$\text{eq. (1)} \quad \mathcal{L}\left[\frac{\partial T}{\partial t}\right] = \mathcal{L}\left[\alpha \frac{\partial^2 T}{\partial x^2}\right]$$

$$\text{if } \bar{T}(x,s) = \mathcal{L}(T) \Rightarrow s\bar{T}(x,s) - T(x,0) = \alpha \frac{\partial^2 \bar{T}}{\partial x^2} \quad (8)$$

$$\text{From (8) and (4)} \quad \frac{\partial^2 \bar{T}}{\partial x^2} - \frac{s}{\alpha} \bar{T} = -\frac{T(x,0)}{\alpha} = -\frac{T_b}{\alpha} \quad (9)$$

Transform of B.C. eq.(2) $\mathcal{L}[T(0,t)] = \bar{T}(0,s) = \frac{T_0}{s}$ (10)

Transform of B.C. eq.(3) $\mathcal{L}[T(\infty,t)] = \bar{T}(\infty,s) = \frac{T_b}{s}$ (11)

Equation (9) becomes an ODE since there are only derivatives with respect to x

Equation (9) is a 2nd-order non-homogeneous ODE.

It's solution is:

$$\bar{T}(x,s) = \underbrace{A(s)e^{\sqrt{\frac{s}{\alpha}}x} + B(s)e^{-\sqrt{\frac{s}{\alpha}}x}}_{\text{homogeneous solution}} + \underbrace{\frac{T_b}{s}}_{\text{particular solution}} \quad (12)$$

Note: A and B are independent of t to satisfy (9)
but they may (may not be dependent on s .

Step 2- satisfy boundary conditions with equation (12)

$$\bar{T}(0, s) = \frac{T_0}{s} = A(s) + B(s) + \frac{T_b}{s} \quad (13)$$

$$\bar{T}(\infty, s) = \frac{T_b}{s} = A(s) e^{\frac{s}{\alpha} \infty} + 0 + \frac{T_b}{s} \quad (14)$$

$$(14) \Rightarrow A(s) = 0 \quad (15)$$

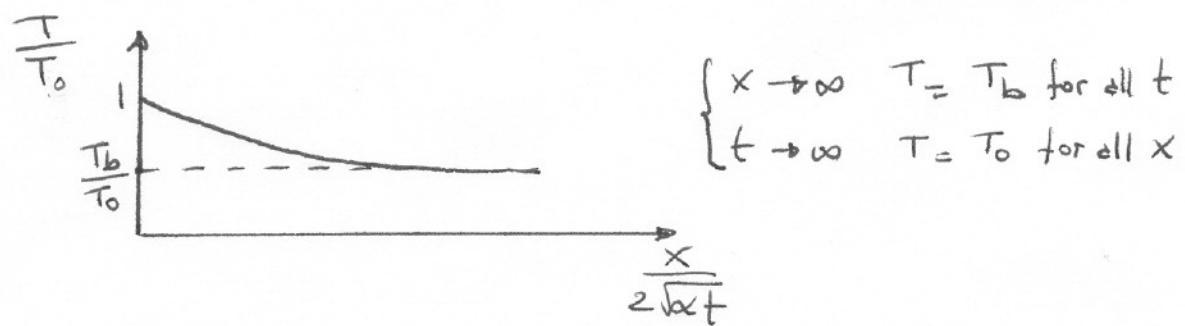
$$(13) \Rightarrow B(s) = \frac{T_0 - T_b}{s} \quad (16)$$

$$\Rightarrow \bar{T}(x, s) = \frac{T_0 - T_b}{s} e^{-\frac{s}{\alpha} x} + \frac{T_b}{s} \quad (17)$$

Step 3- Inverse Laplace (from Tables / Residues)

$$T(x, t) = \mathcal{L}^{-1}(\bar{T}(x, s)) = (T_0 - T_b) \operatorname{erfc}\left(\frac{x}{2\sqrt{\alpha t}}\right) + T_b$$

$$\text{or } \frac{T(x, t)}{T_b} = 1 + \left(\frac{T_b}{T_0} - 1\right) \operatorname{erf}\left(\frac{x}{2\sqrt{\alpha t}}\right)$$



Comments:

- 1- Solution is not in separable form ($f(x)g(t)$)
- 2- x and t collapse into a single variable $x/2\sqrt{\alpha t}$

Example #2: Semi-infinite well with a heat-flux boundary condition.

Semi differential equation $\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial x^2}$ (1)

Initial Condition $T(x, 0) = T_b$ (2)

Boundary Conditions $Q = -K \frac{\partial T}{\partial x} \Big|_{x=0}$ (3)

$T(\infty, t) = T_b$ (4)

Step 1- $\lambda \bar{T}(x, \lambda) - T(x, 0) = \alpha \frac{\partial^2 \bar{T}}{\partial x^2}$ (5)

(Laplace transform of (3)) $\rightarrow K \frac{\partial \bar{T}}{\partial x} = \frac{Q}{\lambda}$ (6)

The solution of (5) is $\bar{T}(x, \lambda) = A(\lambda) e^{-\sqrt{\frac{\lambda}{\alpha}} x} + B(\lambda) e^{\sqrt{\frac{\lambda}{\alpha}} x} + \frac{T_b}{\lambda}$ (7)

Step 2- Satisfy Boundary Conditions with (7)

For $x \rightarrow \infty$, equation (4) $\Rightarrow B e^{\sqrt{\frac{\lambda}{\alpha}} \infty} + \frac{T_b}{\lambda} = \frac{T_b}{\lambda} \Rightarrow B = 0$ (8)

For $x = 0$ $\frac{\partial \bar{T}}{\partial x} \Big|_{x=0} = \frac{Q}{\lambda} = -\sqrt{\frac{\lambda}{\alpha}} A \Rightarrow A(\lambda) = \frac{Q \sqrt{\alpha}}{K \lambda^{3/2}}$ (9)

From (8) and (9) into (7)

$$\bar{T}(x, \lambda) = \frac{Q \sqrt{\alpha}}{K \lambda^{3/2}} e^{-\sqrt{\frac{\lambda}{\alpha}} x} + \frac{T_b}{\lambda} \quad (10)$$

Step 3- Inversion of (10) using Transform Table

$$T(x, t) = \frac{Q \sqrt{\alpha}}{K} \left\{ 2 \sqrt{\frac{t}{\pi}} \exp\left(-\frac{x^2}{4\alpha t}\right) - \frac{x}{\sqrt{\alpha}} \operatorname{erfc}\left(\frac{x}{2\sqrt{\alpha t}}\right) \right\} + T_b$$

Example 3: Steady state Conduction/Convection in a long pipe.

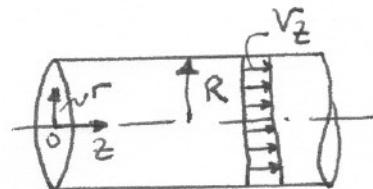
Consider a long horizontal pipe of radius R through which an incompressible fluid is flowing at an average velocity v_z in the z direction.

Assume

$$1 - v_z \gg v_r$$

2 - conduction in r larger than in z .

3 - steady state



The energy equation is $v_z \frac{\partial T}{\partial z} = \alpha \left(\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} \right)$ (1)

$$0 \leq z \leq \infty$$

$$0 \leq r \leq R$$

Solve $T(r, z)$ with Laplace Method. The problem can be also solved by separation of variables.

Boundary Conditions:

$$T(r, 0) = T_0 \quad \text{inlet temperature} \quad (2)$$

$$T(R, z) = T_A \quad \text{ambient temperature} \quad (3)$$

~~Transforming into Laplace space~~

Since the domain is from 0 to ∞ in z , we will do Laplace transform with respect to the z -variable.

Step 1 - Transform the equation and boundary conditions

From (1) $\frac{\partial^2 \bar{T}}{\partial r^2} + \frac{1}{r} \frac{\partial \bar{T}}{\partial r} - \frac{\nu_z}{\alpha} [\delta \bar{T} - T(r, 0)] = 0 \quad (4)$

From (2) and (4) $\frac{\partial^2 \bar{T}}{\partial r^2} + \frac{1}{r} \frac{\partial \bar{T}}{\partial r} - \frac{\nu_z}{\alpha} [\delta \bar{T} - T_0] = 0 \quad (5)$

From (3) $\bar{T}(R, s) = \frac{T_A}{s} \quad (6)$

After algebra, from (5) $\frac{\partial^2 \bar{T}}{\partial r^2} + \frac{1}{r} \frac{\partial \bar{T}}{\partial r} - \frac{\nu_z}{\alpha} \delta \bar{T} = \frac{\nu_z T_0}{\alpha} \quad (7)$

Equation (7) is a nonhomogeneous Modified Bessel Equation:

The solution to the homogeneous part of (7) is:

$$\frac{\partial^2 \bar{T}}{\partial r^2} + \frac{1}{r} \frac{\partial \bar{T}}{\partial r} - \frac{\nu_z}{\alpha} \delta \bar{T} = 0 \Rightarrow \bar{T}(r, s) = A(s) I_0\left(\sqrt{\frac{s\nu_z}{\alpha}} r\right) + B(s) K_0\left(\sqrt{\frac{s\nu_z}{\alpha}} r\right) \quad (8)$$

For the particular solution of (7), by substitution:

$$\frac{\partial^2 \bar{T}}{\partial r^2} + \frac{1}{r} \frac{\partial \bar{T}}{\partial r} - \frac{\nu_z}{\alpha} \delta \bar{T} - \frac{\nu_z T_0}{\alpha} \rightarrow \bar{T} = \frac{1}{s} \cdot T_0 \quad (9)$$

Then, the general solution is:

$$\bar{T}(r, s) = \frac{T_0}{s} + A(s) I_0\left(\sqrt{\frac{s\nu_z}{\alpha}} r\right) + B(s) K_0\left(\sqrt{\frac{s\nu_z}{\alpha}} r\right) \quad (10)$$

Step 2 - Satisfy boundary conditions with equation (10)

Remember, $I_0(r) = J_0(ir)$ and $K_0(r) = Y_0(ir)$

From before $J_0(0) \rightarrow \infty \Rightarrow K_0(0) \rightarrow 0 \Rightarrow$ from (10) $B=0$

Then, from (6) and (10) using $B=0$

$$\frac{T_0}{s} + A(s) I_0\left(\sqrt{\frac{sV_2}{\alpha}} R\right) = \frac{T_A}{s} \Rightarrow A(s) = \frac{T_A - T_0}{s I_0\left(\sqrt{\frac{sV_2}{\alpha}} R\right)} \quad (11)$$

Then, from (11) and (10)

$$\tilde{\tau}(r, s) = \frac{T_0}{s} + \frac{T_A - T_0}{s I_0\left(\sqrt{\frac{sV_2}{\alpha}} R\right)} I_0\left(\sqrt{\frac{sV_2}{\alpha}} r\right) \quad (12)$$

Step 3- Inverse Transform of (12)

The inverse transform is not available in the Laplace Transform Tables.

Then, we have to use a classic result of complex algebra : Cauchy's Theorem of Residues (Proof: Appendix C Rice/Do book)

See review in the next page.

Review : Inversion Theorem with Pole Singularities

Let

$$F(s) = \int_0^\infty f(t) e^{-st} dt$$

Then

$$f(t) = \sum (\text{residues of } F(s) e^{st})$$

Residues are computed as follows:

Assume $s = -a$ is a pole (zero in the denominator of $F(s)$)

Then $\text{res}(s = -a) = [(s+a) F(s) e^{st}] \Big|_{s=-a}$

Simple Example : compute $f(t)$ for:

$$F(s) = \frac{1}{(s+1)(s+2)}$$

$F(s)$ has two poles $s = -1$ $s = -2$

$$\text{residue}(s = -1) = \left[(s+1) \frac{1}{(s+1)(s+2)} e^{st} \right] \Big|_{s=-1} = e^{-t}$$

$$\text{residue}(s = -2) = \left[(s+2) \frac{1}{(s+1)(s+2)} e^{st} \right] \Big|_{s=-2} = -e^{-2t}$$

Then, $f(t) = \sum (\text{residues of } F(s) e^{st})$

$$= e^{-t} - e^{-2t}$$

Now, let complete the pipe problem.

\rightarrow

2nd Simple Example: Residues for $F(s)$ with repeated roots

$$F(s) = \frac{N(s)}{(s-a)^m} \quad \left[\frac{(s-a) N(s)}{(s-a)^m} \cdot e^{st} \right] \Big|_{s=a} \rightarrow \infty$$

multiple roots at $s=a$ (m roots). What are the residues?

If we expand $N(s)$ with a Taylor Series around $s=a$

$$\begin{aligned} N(s) &= N(a) + (s-a)N'(a) + \frac{(s-a)^2}{2!} N''(a) + \dots \\ &\quad + \dots \frac{(s-a)^{m-1}}{(m-1)!} N^{(m-1)}(a) \end{aligned}$$

Let compute:

$$\text{res}(s=a) = \lim_{s \rightarrow a} \left[(s-a) \frac{N(s)}{(s-a)^m} e^{st} \right] = \frac{N^{(m-1)}(a)}{(m-1)!}$$

$$\begin{aligned} F(s) &= \frac{N(s)}{(s-a)^m} \Rightarrow N(s) = F(s) (s-a)^m \\ &\Rightarrow N^{(m-1)}(a) = \left\{ \frac{d^{m-1}}{ds^{m-1}} [F(s) (s-a)^m] \right\} \Big|_{s=a} \end{aligned}$$

$$f(t) = \lim \left[(s-a) \frac{N(s)}{(s-a)^m} e^{st} \right] = \frac{1}{(m-1)!} \left\{ \frac{d^{m-1} [e^{st} F(s) (s-a)^m]}{ds^{m-1}} \right\} \Big|_{s=a}$$

e.g. $\frac{1}{(s-a)^2}$, what is the residue ($s=a$)

$$f(t) = \frac{1}{(2-1)!} t e^{at}$$

Completion of the Long Pipe Problem

$$\text{Invert Eq (12)} \rightarrow \bar{T}(r, s) = \frac{T_0}{s} + \frac{T_A - T_0}{s J_0(\sqrt{\frac{sV_2}{\alpha}} R)} J_0\left(\sqrt{\frac{sV_2}{\alpha}} r\right) \quad (12)$$

Since J_0 is better tabulated than I_0 : use $J_0(i\sqrt{\frac{sV_2}{\alpha}} r) = I_0\left(\sqrt{\frac{sV_2}{\alpha}} r\right)$

$$\text{Then, Define } i\sqrt{\frac{sV_2}{\alpha}} = \lambda \quad (13)$$

Now, equation (12) becomes:

$$\bar{T}(r, s) = \frac{T_0}{s} + \frac{T_A - T_0}{J_0(\lambda R)} J_0(\lambda r) \quad (14)$$

The poles of (14) are $s=0$ and,

from book, the solutions of $J_0(\lambda R) = 0$ λ_n ; $n=1, 2, \dots$

$$\text{Compute residues} \quad \text{from (13)} \quad \Rightarrow \lambda_n = -\lambda_n^2 \frac{\alpha}{V_2} \quad (14.a)$$

$$\text{res}[s=0] = \left[s e^{s\bar{T}} \bar{T}(r, s) \right]_{s=0} = \left\{ e^{s\bar{T}} \left[T_0 + (T_A - T_0) \frac{J_0(\lambda_n r)}{J_0(\lambda_n R)} \right] \right\}_{s=0} = T_A$$

$$\begin{aligned} \text{res}[s=\lambda_n] &= \left[(s-\lambda_n) e^{s\bar{T}} \bar{T}(r, s) \right]_{s=\lambda_n} = \left[(\lambda_n - \lambda_n) e^{s\bar{T}} \left(\frac{T_0}{s} + (T_A - T_0) \frac{J_0(\lambda_n r)}{J_0(\lambda_n R)} \right) \right]_{s=\lambda_n} \\ &= \underbrace{\left[(\lambda_n - \lambda_n) e^{s\bar{T}} \frac{T_0}{s} \right]}_{s=\lambda_n} + \left[(\lambda_n - \lambda_n) e^{s\bar{T}} (T_A - T_0) \frac{J_0(\lambda_n r)}{J_0(\lambda_n R)} \right]_{s=\lambda_n} \end{aligned}$$

However the second term in the last equation = 0 ($r=R$)
 Therefore, we need to apply L'Hopital rule to find limit.

$$= (T_A - T_0) \frac{\frac{d}{ds} \left\{ e^{s^2 (t - \lambda_n)} J_0(\lambda_n r) \right\}_{s=\lambda_n}}{\frac{d}{ds} [s J_0(\lambda_n R)]_{s=\lambda_n}} \frac{\frac{d}{dt} [1 J_0(\lambda_n R)]_{s=\lambda_n}}{\frac{d}{dt} [s J_0(\lambda_n R)]_{s=\lambda_n}} \quad (15)$$

Using a derivation property of Bessel functions:

$$\text{from (13)} \quad \frac{d}{ds} [s J_0(c \sqrt{\frac{\alpha}{\nu t}} R)] = J_0(c \sqrt{\frac{\alpha}{\nu t}} R) - \frac{cR \sqrt{\frac{\alpha}{\nu t}}}{2} J_1(c \sqrt{\frac{\alpha}{\nu t}} R) \\ = -\frac{R}{2} \lambda_n J_1(\lambda_n R) \quad (15) \quad s = \lambda_n$$

from (15) and (16)

$$\Rightarrow \text{res}[s = \lambda_n] = (T_A - T_0) \frac{e^{\lambda_n^2 t} J_0(\lambda_n r)}{-\frac{R}{2} \lambda_n J_1(\lambda_n R)} = -2(T_A - T_0) \frac{e^{-\lambda_n^2 \frac{\alpha}{\nu t} t}}{R \lambda_n} \frac{J_0(\lambda_n r)}{J_1(\lambda_n R)}$$

$$T(r, t) = \sum (\text{residues}) \Rightarrow$$

$$T(r, t) = T_A - \frac{2(T_A - T_0)}{R \lambda_n} \sum_{n=0}^{\infty} e^{-\lambda_n^2 \frac{\alpha}{\nu t} t} \frac{J_0(\lambda_n r)}{J_1(\lambda_n R)}$$

$$\text{For } t \rightarrow \infty \rightarrow e^{-\lambda_n^2 \frac{\alpha}{\nu t} t} = 0 \Rightarrow T(r, t) = T_A$$

It's correct, at the end of the long pipe the liquid exits at ambient temperature.