

Solution: The combined stream function is

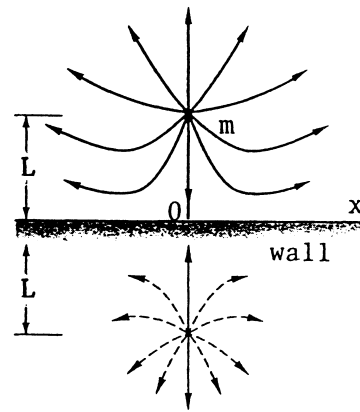
$$\psi = -K \ln(r) - m\theta, \text{ with the angle } \phi \text{ given by}$$

$$\tan \phi = |v_\theta/v_r| = \frac{K/r}{m/r} = \frac{K}{m} = 1.6 \text{ independent of } r, \theta$$

$$\text{The desired angle is } \phi = \tan^{-1}(1.6) \approx 58^\circ \text{ Ans.}$$

Local pressure = 29"Hg = 98 kPa at $V = 75$ m/s, or $r = 25$ meters. Ans.

4.78 We wish to study the flow due to a line source of strength m placed at position $(x, y) = (0, +L)$, above the plane horizontal wall $y = 0$. Using Bernoulli's equation, find (a) the point(s) of minimum pressure on the plane wall and (b) the magnitude of the maximum flow velocity along the wall.



Solution: The "wall" is produced by an image source at $(0, -L)$, as in Prob. 4.68. Along the wall, $y = 0$, $v = 0$, $U = m/L$,

$$u = 2u_{\text{one source}} = \frac{2UL}{(x^2 + L^2)^{1/2}} \cdot \frac{x}{(x^2 + L^2)^{1/2}} = \frac{2ULx}{x^2 + y^2}$$

By differentiation, the maximum velocity occurs at $x = L$, or $u_{\text{max}} = U = \frac{m}{L}$ Ans. (b)

By Bernoulli's equation, this is also the point of minimum pressure, at $(x, y) = (L, 0)$:

$$p_{\text{min}} = p(0, 0) - \frac{1}{2} \rho u_{\text{max}}^2 = p_0 - \frac{1}{2} \rho (m/L)^2 \text{ at } (\pm L, 0) \text{ Ans. (a)}$$

4.79 Study the combined effect of the two viscous flows in Fig. 4.16. That is, find $u(y)$ when the upper plate moves at speed V and there is also a constant pressure gradient (dp/dx). Is superposition possible? If so, explain why. Plot representative velocity profiles for (a) zero, (b) positive, and (c) negative pressure gradients for the same upper-wall speed V .

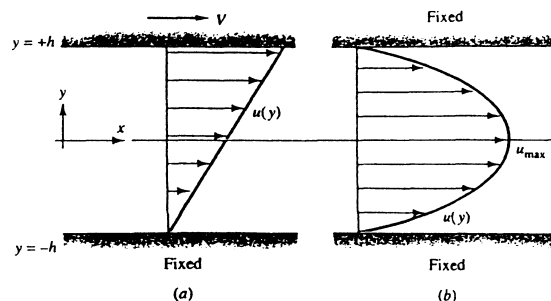


Fig. 4.16

Solution: The combined solution is

$$u = \frac{V}{2} \left(1 + \frac{y}{h} \right) + \frac{h^2}{2\mu} \left(-\frac{dp}{dx} \right) \left(1 - \frac{y^2}{h^2} \right)$$

The superposition is quite valid because the convective acceleration is zero, hence what remains is linear: $\nabla p = \mu \nabla^2 \mathbf{V}$. Three representative velocity profiles are plotted at right for various (dp/dx) .

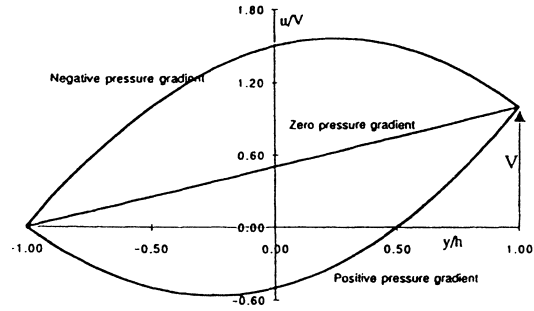
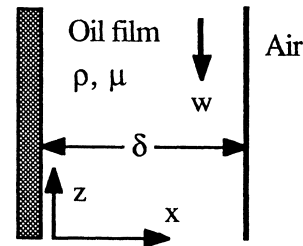


Fig. P4.79

4.80 An oil film drains steadily down the side of a vertical wall, as shown. After an initial development at the top of the wall, the film becomes independent of z and of constant thickness. Assume that $w = w(x)$ only that the atmosphere offers no shear resistance to the film. (a) Solve Navier-Stokes for $w(x)$. (b) Suppose that film thickness and $[\partial w/\partial x]$ at the wall are measured. Find an expression which relates μ to this slope $[\partial w/\partial x]$.



Solution: First, there is no pressure gradient $\partial p/\partial z$ because of the constant-pressure atmosphere. The Navier-Stokes z -component is $\mu d^2w/dx^2 = \rho g$, and the solution requires $w = 0$ at $x = 0$ and $(dw/dx) = 0$ (no shear at the film edge) at $x = \delta$. The solution is:

$$w = \frac{\rho g x}{2\mu} (x - 2\delta) \quad \text{Ans. (a) NOTE: } w \text{ is negative (down)}$$

The wall slope is $\frac{dw}{dx} \Big|_{\text{wall}} = -\frac{\rho g \delta}{\mu}$, or rearrange: $\mu = -\frac{\rho g \delta}{[dw/dx]_{\text{wall}}} \quad \text{Ans. (b)}$

4.81 Modify the analysis of Fig. 4.17 to find the velocity v_θ when the inner cylinder is fixed and the outer cylinder rotates at angular velocity Ω_0 . May this solution be added to Eq. (4.146) to represent the flow caused when both inner and outer cylinders rotate? Explain your conclusion.

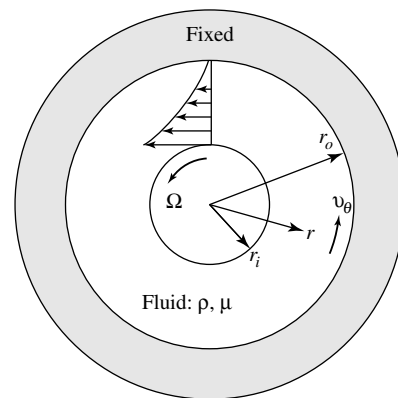


Fig. 4.17

Solution: We apply new boundary conditions to Eq. (4.145) of the text:

$$v_\theta = C_1 r + C_2/r;$$

At $r = r_i, v_\theta = 0 = C_1 r_i + C_2/r_i$